

#### Milan SIGMAFINE SUMMIT 2019 <sup>™</sup> engineering data for digital transformation

## Lost with Losses

### The Hidden Impact of Measurement Technology in Closing Mass Balances

By: Tunahan Avci, Business Development Manager Refining, Blending & Transfer Flow Solutions, Emerson Automation Solutions October 10<sup>th</sup> 2019





Role of Field Instrument accuracy in Production Accounting and Losses

Business Challenges

Using Sigmafine to Identify Measurement Issues

Current Measurement Technologies and Standards

Recommended Practices for Improvement



## **Typical Refinery Losses**

- With **poor** instrumentation and procedures: 1.5-2.5% mass
- With average instrumentation and procedures: 0.7% - 1.5% mass
- With good instrumentation and procedures: < 0.5 % mass
- Good information enhances business functions:
  - Planning and scheduling
  - Process Operations
  - Management Decision



## Mass losses for the overall refinery must be less than 0.5% to meet Solomon Index reporting requirements

Î				
<ul> <li> Upper Management</li> <li>EBITDA</li> <li>Gross Refining Margin</li> <li>Solomon Ranking</li> <li>IIOT</li> </ul>				
<ul> <li> Process Supervisors</li> <li>Throughput</li> <li>Actual vs. Planned</li> <li>Solomon Indices</li> <li>Conversion</li> <li>Energy Costs</li> </ul>				
Operator				
<ul> <li>Flow Measurements</li> <li>Field Measurements</li> <li>Quality Measurements</li> <li>Production rates</li> <li>Temperature</li> </ul>				

## Why Mass Balances Matter



### **Profitability**

- Not overpaying for what you buy or • getting underpaid for what you sell
- You are getting paid for on what • your custody measurement is reading not on your reconciled measurement
- Assurance, control, and validation • of movements (i.e. theft prevention)

### HSE

- Accurate emission reporting to avoid overpaying fines
- Accurate reporting of Energy Intensity Index (EII)
- Ensure not operating above design limits

- **Pinpointing of losses early**
- unaccounted losses
- conversions and yields

### Savings of \$2-10 million per year for an averaged sized refinery



## **Process Optimization**

Identification and minimization of

Unit performance optimization by calculating efficiencies, catalyst



## **Refinery Loss Control Process**



#### Flow measurement is the foundational step for production accounting and loss control

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#### Loss Control Programs

## Case in Point

## Scale of theft at Shell's Singapore refinery much greater, court documents show

Around \$150 million worth of oil was stolen from Shell's biggest global refinery over several years, <u>Singapore</u> court documents reviewed by Reuters show, far more than reported when police first revealed the heist earlier this year.

"Fuel is both ubiquitous and untraceable, making its theft a seemingly low-risk criminal operation compared to something like drug smuggling or arms trafficking, where the concern about being caught is much higher," said Ian Ralby, a maritime crime expert who works with both the U.N. and the U.S.-based



### Shell has taken measures to avoid repeat incidents:

"These include closer monitoring of products moving in and out of Bukom, tightening vessel management procedures, and stepping up ethics and compliance training," the spokeswoman said in an emailed statement to Reuters on Thursday.

### Fuel theft could be worth \$113 billion a year globally, according to industry estimates

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## Challenges With Closing Mass Balances



Accurate flow measurements are key to accurate mass balances

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## **Refinery Plant Wide Mass Balance Challenges**

## **Flow Measurement Challenges**



## **Sources of Error**

- 1. Crude Import Custody **Transfer Measurement**
- 2. Density Measurements
- 3. Natural Gas Measurements
- 4. Fuel Gas
- 5. Inventory Changes

### Additional Sources:

- 1. Coke
- 2. Flare



## Meter Performance from Sigmafine



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![](_page_9_Figure_0.jpeg)

10/30/2019

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## **PiMS**

## **Data Quality KPI - Case**

<b>DX Indicator</b>	Value	Used for ass
DX0 – Redundancy	> 85 %	Sufficiency of flow measur
DX 1 – Imbalance	< 10 %	Overall quality of a set of r
DX 2 – Reconciled Correction	< 5 %	How much correction requ
DX 3 – Tolerance	DX3 > (DX2, DX1)	How well the tolerances a
DX 4 – Reconciled Difference	< 0 (negative)	Level of distortion betwee measured

Generate prescriptions for improving data over time

Classic example: stack ranking of bad meters

## sessing

#### rements

### measurements

### uired to reconcile

### re assigned

### en reconciled and

## **PiMSOfT**

## **Data Quality KPI - Case**

### DX0 – Non redundant data quality indicator

- DX0 =  $1 \Sigma$  Absolute Redundant Mass flows /  $\Sigma$  All absolute mass flows
- Overall percentage of data excluded from the redundancy check

## **DX1 – Imbalance indicator**

- DX1 = RMS (Imbalances) / RMS (Redundant Flows)
- Overall percentage of imbalance in the redundant measurements

### **DX2** - Reconciled Correction Indicator

- DX2 = RMS (Corrections) / RMS (Redundant Flows)
- Amount of adjustments that the solver had to do to satisfy all balances in the plant

### **DX3 – Tolerance Indicator**

- DX3 = RMS (Tolerances) / RMS (Redundant Flows)
- Expected level of overall correction for each day's measurements

### **DX4 – Reconciled Difference Indicator**

- DX4 = RMS (Reconciled Flows) / RMS (Redundant Flows) 1
- Distortion between the reconciled and measured flows

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## **Indirect Benefits of Sigmafine**

Improving & sustaining meter reliability 

![](_page_12_Figure_2.jpeg)

## **PiMS**

## **Custody Measurement Types**

- Mass and Volumetric Flow Meters
- Automatic Tank Gauges (ATG)
- Marine Vessel Gauging
- Manual Gauging
- Truck and Rail Car Outages
- Weigh Scales

![](_page_13_Picture_7.jpeg)

![](_page_13_Picture_8.jpeg)

## **Distribution of Flowmeter Technology**

![](_page_14_Figure_1.jpeg)

![](_page_14_Picture_2.jpeg)

## Historical Practice for Mass Balance Meters – Use Volumetric Technologies

### **Orifice dP Meters for Process Applications**

#### **Advantages**

- Greatest application flexibility
- Low purchase price
  - Independent of line size
  - Cost effective for larger line sizes

### Limitations

- Poor accuracy when uncompensated, 1-5%
- Moderate accuracy when compensated: 0.5-1.5%
  - Having a known fluid density is the key to achieving this accuracy
- Accuracy degraded by orifice plate wear, difficult to detecf
- Impulse lines can plug

![](_page_15_Picture_13.jpeg)

#### **Mechanical Meters for Custody Transfer Applications**

- Metering performance affected by fluid properties
- Extensive moving/wearing parts
  - High maintenance
  - Meter factor shift
- NEED to be frequently checked and adjusted

![](_page_15_Figure_20.jpeg)

![](_page_15_Picture_21.jpeg)

![](_page_15_Picture_26.jpeg)

## Coriolis Meters Eliminate The Largest Sources of Measurement Error in Mass **Balance and Custody Transfer Applications**

- Direct Mass and Density Measurement
  - Not affected by changes in composition, viscosity, temperate, pressure, conductivity
- Rangeability
  - 20:1 for custody
  - 100:1 for non-custody

### Measurement accuracy

- At 20:1 turndown:
  - Mass Flow Rate: ±0.1 (optional 0.05 %)
  - Volume Flow Rate: ±0.1% (optional 0.05%)
- No flow conditioning or straight runs required
  - Not dependent on flow profile

- Measures difficult and/or viscous fluids Liquid asphalt and molten sulfur
- Bi-directional Measurement
- Low Maintenance No moving parts

### Two-Phase Flow Indication

- Provides notification of the fluid being single phase, moderate entrainment, and severe entrainment
- Smart Meter Verification (SMV)
  - In-situation testing of meter integrity tube stiffness, sensor components, transmitter electronics
  - Extend calibration cycles

![](_page_16_Picture_23.jpeg)

## Long Term Meter Factor Stability

![](_page_17_Figure_1.jpeg)

Compact Prover on LPG in refinery in Brazil.

## Smart Meter Verification Delivers Confidence in Measurement

![](_page_18_Figure_1.jpeg)

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![](_page_18_Picture_4.jpeg)

## **Standards for Coriolis Meters**

Manual of Petroleum **Measurement Standards** Chapter 5—Metering

Section 6—Measurement of Liquid Hydrocarbons by Coriolis Meters

Measurement Coordination

FIRST EDITION, OCTOBER 2002

![](_page_19_Picture_5.jpeg)

![](_page_19_Picture_6.jpeg)

Petroleum Institute

**Helping You Get The Job** Done Right.

![](_page_19_Picture_9.jpeg)

![](_page_19_Picture_10.jpeg)

![](_page_19_Picture_12.jpeg)

![](_page_19_Picture_13.jpeg)

## Example: Tanker Lightering using Coriolis

![](_page_20_Picture_1.jpeg)

## Common Sources of Error for Refinery Mass Balance Flare Measurement

### Flare

- Losses through flare are typically the largest source of identifiable loss
- Measurement challenges:
  - Wide turndown requirements
  - Widely changing compositions
  - Very low gas pressure
  - Fully developed flow profile at low end difficult
- Uncertainty is often above 10% at the low end but technology advances can significantly improve that performance
- Measurement technology:
  - Ultrasonic meters + Gas composition analysis either by lab sampling, GC or Mass Spectrometry
  - Technology enhancements for ultrasonic meters resulting in improved accuracy
    - MW calculations using sound speed of the gas
    - Correction factors from computational fluid dynamics

![](_page_21_Figure_14.jpeg)

## Custody Transfer and Inventory Tracking – ATG (Radar)

- For the calculation of a transferred quantity the tank gauging system requires:
  - Level, at start and end of transfer
  - Average product temperature, at start and end of transfer
  - **Density** (or API gravity), at start and end of transfer.
  - Base Sediment & Water
  - Tank Strapping Table

![](_page_22_Picture_7.jpeg)

## Accuracy of Automatic Tank Gauging

![](_page_23_Figure_1.jpeg)

1 API ± 3/16" (4 mm)	Manual
2 PTB, Germany	Chapter
3 NMi, Netherlands	Section 1B
4 OIML, International	
5 TankRadar	

#### APPENDIX B—ACCURACY REQUIREMENTS FOR ATG (See Note)

Requirement	Custody Transfer	
Factory calibration	$1 \text{ mm} (^{1}/_{16} \text{ inch})$	3 r
Effect of installation	$3 \text{ mm} (^{1}/_{8} \text{ inch})$	
Initial verification	$4 \text{ mm} (^{3}/_{16} \text{ inch})$	25
Subsequent verification	$4 \text{ mm} (^{3}/_{16} \text{ inch})$	25
Frequency of verification	monthly	
Note: This table is for refere	nce only. Please refer to th	e entire

#### of Petroleum rement Standards r 3—Tank Gauging

B—Standard Practice for Level Measurement of Liquid Hydrocarbons in Stationary Tanks by Automatic Tank Gauging

Inventory

mm  $(1/_8 \text{ inch})$ 

n.a.

mm (1 inch)

mm (1 inch)

quarterly

document.

American Petroleum Institute 1220 L Street, Northwest Washington, D.C. 20005

# Uncertainty of Tank Volumes and Mass is highly dependent on instrumentation and maintenance of the tank

- Tank Gauging System Installation Method
- Uncertainty in Tank Capacity Table
  - Calibration method
  - Maintenance of strapping table
- Uncertainty in Average Product Temperature
  - Multi-spot
- Uncertainty in Density Measurement
  - Manual sampling (sampling procedure and laboratory)
  - Automatic (precision of the pressure transducer)
  - Stratification of fluid in the tank

![](_page_24_Picture_11.jpeg)

## How to Improve Mass Balances

### Evaluate your current closure of your mass balances

- How does your refinery wide balance compare to your target or expected benchmarks?
- Are there some process units that are more difficult to close?

### Use Sigmafine to identify measurement issues

KPI's to evaluate current systems and help to prioritize

### Critical balance points to prioritize

- Crude import
- Crude charge to the crude unit
- Conversion unit feed rates
- Primary products for accurate yield data
- Unconverted bottoms

### Perform an audit of prioritized measurements

Understand contributions to measurement uncertainty and the overall accuracy and possible biases

![](_page_25_Picture_16.jpeg)

## Key Takeaways

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## **Thank You**

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